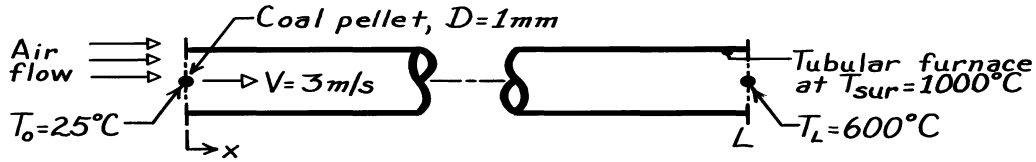


### PROBLEM 5.32

**KNOWN:** Spherical coal pellet at 25°C is heated by radiation while flowing through a furnace maintained at 1000°C.

**FIND:** Length of tube required to heat pellet to 600°C.

**SCHEMATIC:**



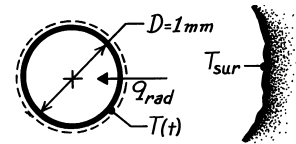
**ASSUMPTIONS:** (1) Pellet is suspended in air flow and subjected to only radiative exchange with furnace, (2) Pellet is small compared to furnace surface area, (3) Coal pellet has emissivity,  $\epsilon = 1$ .

**PROPERTIES:** Table A-3, Coal ( $\bar{T} = (600 + 25)^\circ\text{C}/2 = 585\text{K}$ , however, only 300K data available):  $\rho = 1350 \text{ kg/m}^3$ ,  $c_p = 1260 \text{ J/kg}\cdot\text{K}$ ,  $k = 0.26 \text{ W/m}\cdot\text{K}$ .

**ANALYSIS:** Considering the pellet as spatially isothermal, use the lumped capacitance method of Section 5.3 to find the time required to heat the pellet from  $T_o = 25^\circ\text{C}$  to  $T_L = 600^\circ\text{C}$ . From an energy balance on the pellet  $\dot{E}_{\text{in}} = \dot{E}_{\text{st}}$  where

$$\dot{E}_{\text{in}} = q_{\text{rad}} = \sigma A_s (T_{\text{sur}}^4 - T_s^4) \quad \dot{E}_{\text{st}} = \rho \forall c_p \frac{dT}{dt}$$

giving  $A_s \sigma (T_{\text{sur}}^4 - T_s^4) = \rho \forall c_p \frac{dT}{dt}$ .



Separating variables and integrating with limits shown, the temperature-time relation becomes

$$\frac{A_s \sigma}{\rho \forall c_p} \int_0^t dt = \int_{T_o}^{T_L} \frac{dT}{T_{\text{sur}}^4 - T^4}.$$

The integrals are evaluated in Eq. 5.18 giving

$$t = \frac{\rho \forall c_p}{4 A_s \sigma T_{\text{sur}}^3} \left\{ \ln \left| \frac{T_{\text{sur}} + T}{T_{\text{sur}} - T} \right| - \ln \left| \frac{T_{\text{sur}} + T_i}{T_{\text{sur}} - T_i} \right| + 2 \left[ \tan^{-1} \left[ \frac{T}{T_{\text{sur}}} \right] - \tan^{-1} \left[ \frac{T_i}{T_{\text{sur}}} \right] \right] \right\}.$$

Recognizing that  $A_s = \pi D^2$  and  $\forall = \pi D^3/6$  or  $A_s/\forall = 6/D$  and substituting values,

$$t = \frac{1350 \text{ kg/m}^3 (0.001 \text{ m}) 1260 \text{ J/kg}\cdot\text{K}}{24 \times 5.67 \times 10^{-8} \text{ W/m}^2 \cdot \text{K}^4 (1273 \text{ K})^3} \left\{ \ln \frac{1273 + 873}{1273 - 873} - \ln \frac{1273 + 298}{1273 - 298} + 2 \left[ \tan^{-1} \left( \frac{873}{1273} \right) - \tan^{-1} \left( \frac{298}{1273} \right) \right] \right\} = 1.18 \text{ s}.$$

Hence,  $L = V \cdot t = 3 \text{ m/s} \times 1.18 \text{ s} = 3.54 \text{ m}$ .

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The validity of the lumped capacitance method requires  $Bi = h(\forall/A_s)/k < 0.1$ . Using Eq. (1.9) for  $h = h_r$  and  $\forall/A_s = D/6$ , find that when  $T = 600^\circ\text{C}$ ,  $Bi = 0.19$ ; but when  $T = 25^\circ\text{C}$ ,  $Bi = 0.10$ . At early times, when the pellet is cooler, the assumption is reasonable but becomes less appropriate as the pellet heats.