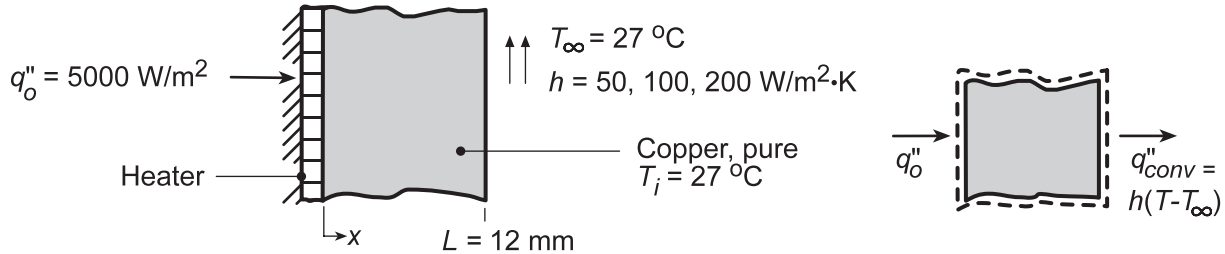


### PROBLEM 5.30

**KNOWN:** Electrical heater attached to backside of plate while front is exposed to a convection process ( $T_\infty, h$ ); initially plate is at uniform temperature  $T_\infty$  before heater power is switched on.

**FIND:** (a) Expression for temperature of plate as a function of time assuming plate is spacewise isothermal, (b) Approximate time to reach steady-state and  $T(\infty)$  for prescribed  $T_\infty, h$  and  $q_o''$  when wall material is pure copper, (c) Effect of  $h$  on thermal response.

**SCHEMATIC:**



**ASSUMPTIONS:** (1) Plate behaves as lumped capacitance, (2) Negligible loss out backside of heater, (3) Negligible radiation, (4) Constant properties.

**PROPERTIES:** Table A-1, Copper, pure (350 K):  $k = 397 \text{ W/m}\cdot\text{K}$ ,  $c_p = 385 \text{ J/kg}\cdot\text{K}$ ,  $\rho = 8933 \text{ kg/m}^3$ .

**ANALYSIS:** (a) Following the analysis of Section 5.3, the energy conservation requirement for the system is  $\dot{E}_{\text{in}} - \dot{E}_{\text{out}} = \dot{E}_{\text{st}}$  or  $q_o'' - h(T - T_\infty) = \rho L c_p dT/dt$ . Rearranging, and with  $R_t'' = 1/h$  and  $C_t'' = \rho L c_p$ ,

$$T - T_\infty - q_o''/h = -R_t'' \cdot C_t'' dT/dt \quad (1)$$

Defining  $\theta(t) \equiv T - T_\infty - q_o''/h$  with  $d\theta = dT$ , the differential equation is

$$\theta = -R_t'' C_t'' \frac{d\theta}{dt} \quad (2)$$

Separating variables and integrating,

$$\int_{\theta_i}^{\theta} \frac{d\theta}{\theta} = - \int_0^t \frac{dt}{R_t'' C_t''}$$

it follows that

$$\frac{\theta}{\theta_i} = \exp\left(-\frac{t}{R_t'' C_t''}\right) \quad (3)$$

where  $\theta_i = \theta(0) = T_i - T_\infty - (q_o''/h)$  (4)

(b) For  $h = 50 \text{ W/m}^2 \cdot \text{K}$ , the steady-state temperature can be determined from Eq. (3) with  $t \rightarrow \infty$ ; that is,

$$\theta(\infty) = 0 = T(\infty) - T_\infty - q_o''/h \quad \text{or} \quad T(\infty) = T_\infty + q_o''/h,$$

giving  $T(\infty) = 27^\circ\text{C} + 5000 \text{ W/m}^2 / 50 \text{ W/m}^2 \cdot \text{K} = 127^\circ\text{C}$ . To estimate the time to reach steady-state, first determine the thermal time constant of the system,

$$\tau_t = R_t'' C_t'' = \left(\frac{1}{h}\right) (\rho c_p L) = \left(\frac{1}{50 \text{ W/m}^2 \cdot \text{K}}\right) (8933 \text{ kg/m}^3 \times 385 \text{ J/kg} \cdot \text{K} \times 12 \times 10^{-3} \text{ m}) = 825 \text{ s}$$

Continued...

### PROBLEM 5.30 (Cont.)

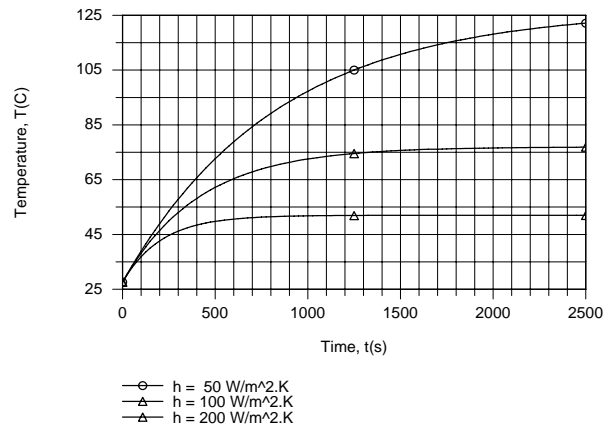
When  $t = 3\tau_t = 3 \times 825 \text{ s} = 2475 \text{ s}$ , Eqs. (3) and (4) yield

$$\theta(3\tau_t) = T(3\tau_t) - 27^\circ\text{C} - \frac{5000 \text{ W/m}^2}{50 \text{ W/m}^2 \cdot \text{K}} = e^{-3} \left[ 27^\circ\text{C} - 27^\circ\text{C} - \frac{5000 \text{ W/m}^2}{50 \text{ W/m}^2 \cdot \text{K}} \right]$$

$$T(3\tau_t) = 122^\circ\text{C}$$

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(c) As shown by the following graphical results, which were generated using the IHT *Lumped Capacitance Model*, the steady-state temperature and the time to reach steady-state both decrease with increasing  $h$ .



**COMMENTS:** Note that, even for  $h = 200 \text{ W/m}^2 \cdot \text{K}$ ,  $\text{Bi} = hL/k \ll 0.1$  and assumption (1) is reasonable.