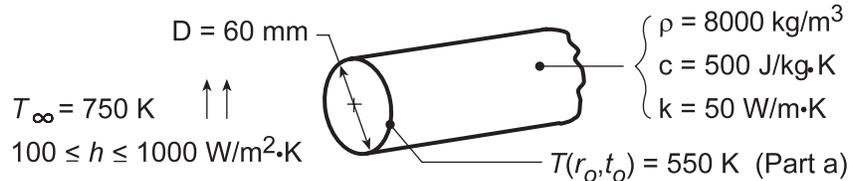


## PROBLEM 5.60

**KNOWN:** Long rod with prescribed diameter and properties, initially at a uniform temperature, is heated in a forced convection furnace maintained at 750 K with a convection coefficient of  $h = 1000 \text{ W/m}^2\cdot\text{K}$ .

**FIND:** (a) The corresponding center temperature of the rod,  $T(0, t_0)$ , when the surface temperature  $T(r_0, t_0)$  is measured as 550 K, (b) Effect of  $h$  on centerline temperature history.

**SCHEMATIC:**



**ASSUMPTIONS:** (1) One-dimensional, radial conduction in rod, (2) Constant properties, (3) Rod, when initially placed in furnace, had a uniform (but unknown) temperature, (4)  $Fo \geq 0.2$ .

**ANALYSIS:** (a) Since the rod was initially at a uniform temperature and  $Fo \geq 0.2$ , the approximate solution for the infinite cylinder is appropriate. From Eq. 5.52b,

$$\theta^*(r^*, Fo) = \theta_o^*(Fo) J_0(\zeta_1 r^*) \quad (1)$$

where, for  $r^* = 1$ , the dimensionless temperatures are, from Eq. 5.34,

$$\theta^*(1, Fo) = \frac{T(r_0, t_0) - T_\infty}{T_i - T_\infty} \quad \theta_o^*(Fo) = \frac{T(0, t_0) - T_\infty}{T_i - T_\infty} \quad (2,3)$$

Combining Eqs. (2) and (3) with Eq. (1) and rearranging,

$$\begin{aligned} \frac{T(r_0, t_0) - T_\infty}{T_i - T_\infty} &= \frac{T(0, t_0) - T_\infty}{T_i - T_\infty} J_0(\zeta_1 \cdot 1) \\ T(0, t_0) &= T_\infty + \frac{1}{J_0(\zeta_1)} [T(r_0, t_0) - T_\infty] \end{aligned} \quad (4)$$

The eigenvalue,  $\zeta_1 = 1.0185 \text{ rad}$ , follows from Table 5.1 for the Biot number

$$Bi = \frac{hr_0}{k} = \frac{1000 \text{ W/m}^2 \cdot \text{K} (0.060 \text{ m}/2)}{50 \text{ W/m} \cdot \text{K}} = 0.60.$$

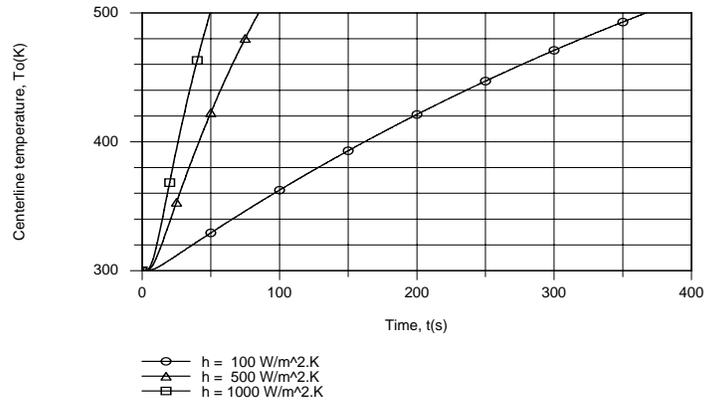
From Table B-4, with  $\zeta_1 = 1.0185 \text{ rad}$ ,  $J_0(1.0185) = 0.7568$ . Hence, from Eq. (4)

$$T(0, t_0) = 750 \text{ K} + \frac{1}{0.7568} [550 - 750] \text{ K} = 486 \text{ K} \quad <$$

(b) Using the IHT *Transient Conduction Model for a Cylinder*, the following temperature histories were generated.

Continued...

### PROBLEM 5.60 (Cont.)



The times required to reach a centerline temperature of 500 K are 367, 85 and 51s, respectively, for  $h = 100, 500$  and  $1000 \text{ W/m}^2\cdot\text{K}$ . The corresponding values of the Biot number are 0.06, 0.30 and 0.60. Hence, even for  $h = 1000 \text{ W/m}^2\cdot\text{K}$ , the convection resistance is not negligible relative to the conduction resistance and significant reductions in the heating time could still be effected by increasing  $h$  to values considerably in excess of  $1000 \text{ W/m}^2\cdot\text{K}$ .

**COMMENTS:** For Part (a), recognize why it is not necessary to know  $T_i$  or the time  $t_0$ . We require that  $Bi \geq 0.2$ , which for this sphere corresponds to  $t \geq 14\text{s}$ . For this situation, the time dependence of the surface and center are the same.