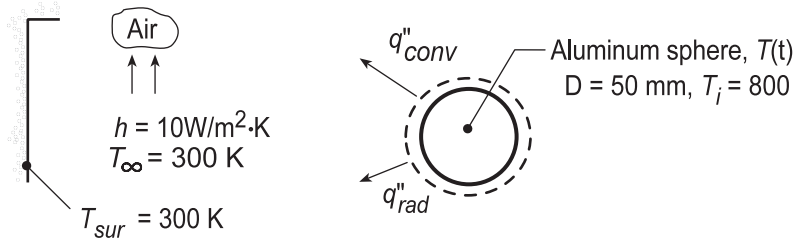


### PROBLEM 5.34

**KNOWN:** Metal sphere, initially at a uniform temperature  $T_i$ , is suddenly removed from a furnace and suspended in a large room and subjected to a convection process ( $T_\infty$ ,  $h$ ) and to radiation exchange with surroundings,  $T_{sur}$ .

**FIND:** (a) Time it takes for sphere to cool to some temperature  $T$ , neglecting radiation exchange, (b) Time it takes for sphere to cool to some temperature  $t$ , neglecting convection, (c) Procedure to obtain time required if both convection and radiation are considered, (d) Time to cool an anodized aluminum sphere to 400 K using results of Parts (a), (b) and (c).

**SCHEMATIC:**



**ASSUMPTIONS:** (1) Sphere is spacewise isothermal, (2) Constant properties, (3) Constant heat transfer convection coefficient, (4) Sphere is small compared to surroundings.

**PROPERTIES:** Table A-1, Aluminum, pure ( $\bar{T} = [800 + 400] \text{ K}/2 = 600 \text{ K}$ ):  $\rho = 2702 \text{ kg/m}^3$ ,  $c = 1033 \text{ J/kg}\cdot\text{K}$ ,  $k = 231 \text{ W/m}\cdot\text{K}$ ,  $\alpha = k/\rho c = 8.276 \times 10^{-5} \text{ m}^2/\text{s}$ ; Aluminum, anodized finish:  $\varepsilon = 0.75$ , polished surface:  $\varepsilon = 0.1$ .

**ANALYSIS:** (a) Neglecting radiation, the time to cool is predicted by Eq. 5.5,

$$t = \frac{\rho V c}{h A_s} \ln \frac{\theta_i}{\theta} = \frac{\rho D c}{6 h} \ln \frac{T_i - T_\infty}{T - T_\infty} \quad (1) <$$

where  $V/A_s = (\pi D^3/6)/(\pi D^2) = D/6$  for the sphere.

(b) Neglecting convection, the time to cool is predicted by Eq. 5.18,

$$t = \frac{\rho D c}{24 \varepsilon \sigma T_{sur}^3} \left\{ \ln \left| \frac{T_{sur} + T}{T_{sur} - T} \right| - \ln \left| \frac{T_{sur} + T_i}{T_{sur} - T_i} \right| + 2 \left[ \tan^{-1} \left( \frac{T}{T_{sur}} \right) - \tan^{-1} \left( \frac{T_i}{T_{sur}} \right) \right] \right\} \quad (2)$$

where  $V/A_{s,r} = D/6$  for the sphere.

(c) If convection and radiation exchange are considered, the energy balance requirement results in Eq. 5.15 (with  $\dot{q}_s'' = \dot{E}_g = 0$ ). Hence

$$\frac{dT}{dt} = \frac{6}{\rho D c} \left[ h(T - T_\infty) + \varepsilon \sigma (T^4 - T_{sur}^4) \right] \quad (3) <$$

where  $A_{s(c,r)} = A_s = \pi D^2$  and  $V/A_{s(c,r)} = D/6$ . This relation must be solved numerically in order to evaluate the time-to-cool.

(d) For the aluminum (pure) sphere with an anodized finish and the prescribed conditions, the times to cool from  $T_i = 800 \text{ K}$  to  $T = 400 \text{ K}$  are:

Continued...

### PROBLEM 5.34 (Cont.)

Convection only, Eq. (1)

$$t = \frac{2702 \text{ kg/m}^3 \times 0.050 \text{ m} \times 1033 \text{ J/kg} \cdot \text{K}}{6 \times 10 \text{ W/m}^2 \cdot \text{K}} \ln \frac{800 - 300}{400 - 300} = 3743 \text{ s} = 1.04 \text{ h}$$

<

Radiation only, Eq. (2)

$$t = \frac{2702 \text{ kg/m}^3 \times 0.050 \text{ m} \times 1033 \text{ J/kg} \cdot \text{K}}{24 \times 0.75 \times 5.67 \times 10^{-8} \text{ W/m}^2 \cdot \text{K}^4 \times (300 \text{ K})^3} \cdot \left\{ \left( \ln \frac{400 + 300}{400 - 300} - \ln \frac{800 + 300}{800 - 300} \right) + 2 \left[ \tan^{-1} \frac{400}{300} - \tan^{-1} \frac{800}{300} \right] \right\}$$

$$t = 5.065 \times 10^3 \{ 1.946 - 0.789 + 2(0.927 - 1.212) \} = 2973 \text{ s} = 0.826 \text{ h}$$

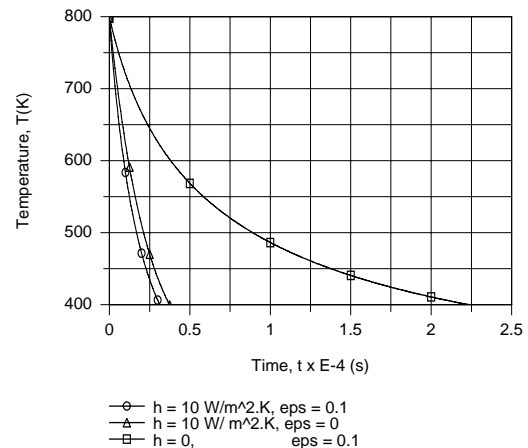
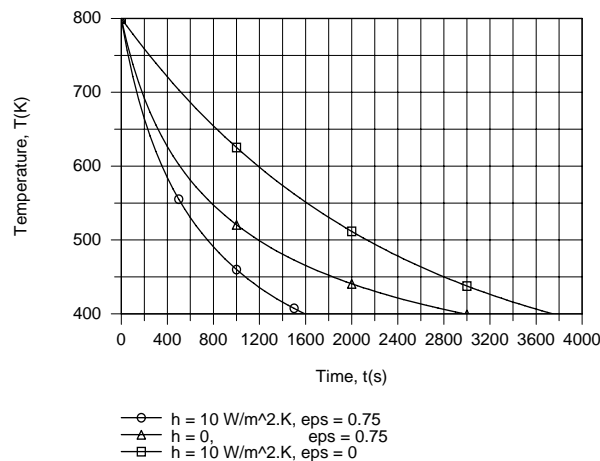
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Radiation and convection, Eq. (3)

Using the IHT Lumped Capacitance Model, numerical integration yields

$$t \approx 1600 \text{ s} = 0.444 \text{ h}$$

In this case, heat loss by radiation exerts the stronger influence, although the effects of convection are by no means negligible. However, if the surface is polished ( $\epsilon = 0.1$ ), convection clearly dominates. For each surface finish and the three cases, the temperature histories are as follows.



**COMMENTS:** 1. A summary of the analyses shows the relative importance of the various modes of heat loss:

Active Modes	Time required to cool to 400 K (h)	
	$\epsilon = 0.75$	$\epsilon = 0.1$
Convection only	1.040	1.040
Radiation only	0.827	6.194
Both modes	0.444	0.889

2. Note that the spacewise isothermal assumption is justified since  $Be \ll 0.1$ . For the convection-only process,

$$Bi = h(r_o/3)/k = 10 \text{ W/m}^2 \cdot \text{K} (0.025 \text{ m}/3) / 231 \text{ W/m} \cdot \text{K} = 3.6 \times 10^{-4}$$