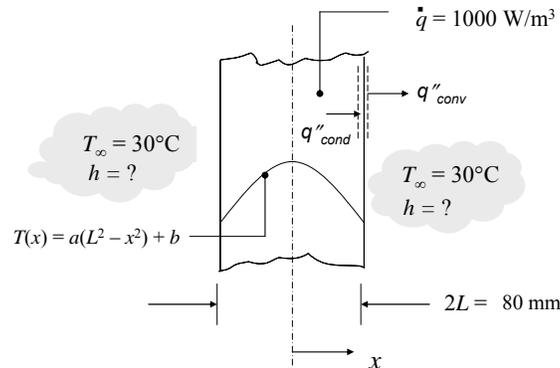


## PROBLEM 2.10

**KNOWN:** Wall thickness. Thermal energy generation rate. Temperature distribution. Ambient fluid temperature.

**FIND:** Thermal conductivity. Convection heat transfer coefficient.

**SCHEMATIC:**



**ASSUMPTIONS:** (1) Steady state, (2) One-dimensional conduction, (3) Constant properties, (4) Negligible radiation.

**ANALYSIS:** Under the specified conditions, the heat equation, Equation 2.21, reduces to

$$\frac{d^2T}{dx^2} + \frac{\dot{q}}{k} = 0$$

With the given temperature distribution,  $d^2T/dx^2 = -2a$ . Therefore, solving for  $k$  gives

$$k = \frac{\dot{q}}{2a} = \frac{1000 \text{ W/m}^3}{2 \times 15^\circ\text{C/m}^2} = 33.3 \text{ W/m} \cdot \text{K} \quad <$$

The convection heat transfer coefficient can be found by applying the boundary condition at  $x = L$  (or at  $x = -L$ ),

$$-k \left. \frac{dT}{dx} \right|_{x=L} = h[T(L) - T_\infty]$$

Therefore

$$h = \frac{-k \left. \frac{dT}{dx} \right|_{x=L}}{[T(L) - T_\infty]} = \frac{2kaL}{b - T_\infty} = \frac{2 \times 33.3 \text{ W/m} \cdot \text{K} \times 15^\circ\text{C/m}^2 \times 0.04 \text{ m}}{40^\circ\text{C} - 30^\circ\text{C}} = 4 \text{ W/m}^2 \cdot \text{K} \quad <$$

**COMMENTS:** (1) In Chapter 3, you will learn how to determine the temperature distribution. (2) The heat transfer coefficient could also have been found from an energy balance on the wall. With  $\dot{E}_{\text{in}} - \dot{E}_{\text{out}} + \dot{E}_g = 0$ , we find  $-2hA[T(L) - T_\infty] + 2\dot{q}LA = 0$ . This yields the same result for  $h$ .