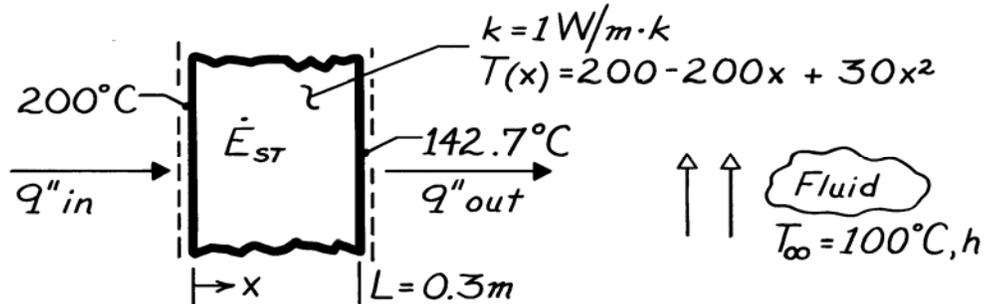


PROBLEM 2.31

KNOWN: Wall thickness, thermal conductivity, temperature distribution, and fluid temperature.

FIND: (a) Surface heat rates and rate of change of wall energy storage per unit area, and (b) Convection coefficient.

SCHEMATIC:



ASSUMPTIONS: (1) One-dimensional conduction in x , (2) Constant k .

ANALYSIS: (a) From Fourier's law,

$$q''_x = -k \frac{\partial T}{\partial x} = (200 - 60x) \cdot k$$

$$q''_{in} = q''_{x=0} = 200 \frac{^\circ\text{C}}{\text{m}} \times 1 \frac{\text{W}}{\text{m} \cdot \text{K}} = 200 \text{ W/m}^2 \quad <$$

$$q''_{out} = q''_{x=L} = (200 - 60 \times 0.3)^\circ\text{C/m} \times 1 \text{ W/m} \cdot \text{K} = 182 \text{ W/m}^2. \quad <$$

Applying an energy balance to a control volume about the wall, Eq. 1.12c,

$$\dot{E}''_{in} - \dot{E}''_{out} = \dot{E}''_{st}$$

$$\dot{E}''_{st} = q''_{in} - q''_{out} = 18 \text{ W/m}^2. \quad <$$

(b) Applying a surface energy balance at $x = L$,

$$q''_{out} = h [T(L) - T_\infty]$$

$$h = \frac{q''_{out}}{T(L) - T_\infty} = \frac{182 \text{ W/m}^2}{(142.7 - 100)^\circ\text{C}}$$

$$h = 4.3 \text{ W/m}^2 \cdot \text{K}. \quad <$$

COMMENTS: (1) From the heat equation,

$$(\partial T / \partial t) = (k / \rho c_p) \partial^2 T / \partial x^2 = 60(k / \rho c_p),$$

it follows that the temperature is increasing with time at every point in the wall.

(2) The value of h is small and is typical of free convection in a gas.