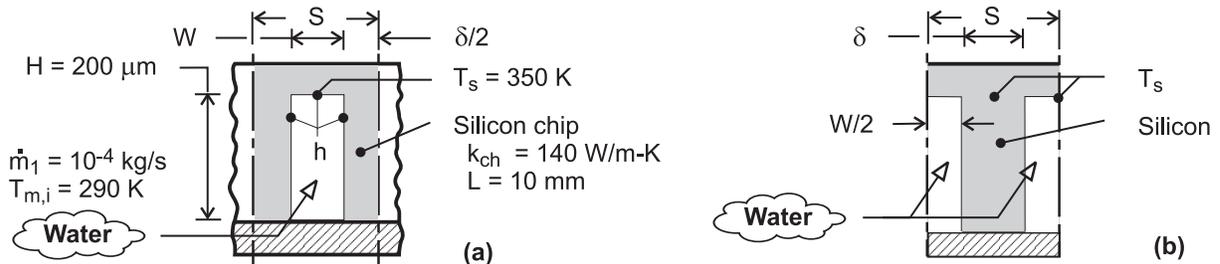


PROBLEM 8.109

KNOWN: Chip and cooling channel dimensions. Channel flow rate and inlet temperature. Temperature of chip at base of channel.

FIND: (a) Water outlet temperature and chip power, (b) Effect of channel width and pitch on power dissipation.

SCHEMATIC:



ASSUMPTIONS: (1) Incompressible liquid with negligible viscous dissipation, (2) Flow may be approximated as fully developed and channel walls as isothermal for purposes of estimating the convection coefficient, (3) One-dimensional conduction along channel side walls, (4) Adiabatic condition at end of side walls, (5) Heat dissipation is exclusively through fluid flow in channels, (6) Constant properties.

PROPERTIES: Table A-6, Water ($\bar{T}_m = 300\text{K}$): $c_p = 4179\text{ J/kg}\cdot\text{K}$, $\mu = 855 \times 10^{-6}\text{ kg/s}\cdot\text{m}$, $k = 0.613\text{ W/m}\cdot\text{K}$, $Pr = 5.83$.

ANALYSIS: (a) The channel sidewalls act as fins, and a *unit* channel/sidewall combination is shown in schematic (a), where the total number of unit cells corresponds to $N = L/S$. With $N = 50$ and $L = 10\text{ mm}$, $S = 200\ \mu\text{m}$ and $\delta = S - W = 150\ \mu\text{m}$. Alternatively, the unit cell may be represented in terms of a single fin of thickness δ , as shown in schematic (b). The thermal resistance of the unit cell may be obtained from the expression for a fin array, Eq. (3.108), $R_{t,o} = (\eta_o h A_t)^{-1}$, where $A_t = A_f + A_b = L(2H + W) = 0.01\text{m}(4 \times 10^{-4} + 0.5 \times 10^{-4})\text{ m} = 4.5 \times 10^{-6}\text{ m}^2$. With $D_h = 4(H \times W)/2(H + W) = 4(2 \times 10^{-4}\text{ m} \times 0.5 \times 10^{-4}\text{ m})/2(2.5 \times 10^{-4}\text{ m}) = 8 \times 10^{-5}\text{ m}$, the Reynolds number is $Re_D = \rho u_m D_h/\mu = \dot{m}_1 D_h/A_c \mu = 10^{-4}\text{ kg/s} \times 8 \times 10^{-5}\text{ m}/(2 \times 10^{-4}\text{ m} \times 0.5 \times 10^{-4}\text{ m}) 855 \times 10^{-6}\text{ kg/s}\cdot\text{m} = 936$. Hence, the flow is laminar, and assuming fully developed conditions throughout a channel with uniform surface temperature, Table 8.1 yields $Nu_D = 4.44$. Hence,

$$h = \frac{k}{D_h} Nu_D = \frac{0.613\text{ W/m}\cdot\text{K} \times 4.44}{8 \times 10^{-5}\text{ m}} = 34,022\text{ W/m}^2 \cdot \text{K}$$

With $m = (2h/k_{ch}\delta)^{1/2} = (68,044\text{ W/m}^2 \cdot \text{K}/140\text{ W/m}\cdot\text{K} \times 1.5 \times 10^{-4}\text{ m})^{1/2} = 1800\text{ m}^{-1}$ and $mH = 0.36$, the fin efficiency is

$$\eta_f = \frac{\tanh mH}{mH} = \frac{0.345}{0.36} = 0.958$$

and the overall surface efficiency is

$$\eta_o = 1 - \frac{A_f}{A_t}(1 - \eta_f) = 1 - \frac{4.0 \times 10^{-6}}{4.5 \times 10^{-6}}(1 - 0.958) = 0.963$$

The thermal resistance of the unit cell is then

Continued ...

PROBLEM 8.109 (Cont.)

$$R_{t,o} = (\eta_o h A_t)^{-1} = \left(0.963 \times 34,022 \text{ W/m}^2 \cdot \text{K} \times 4.5 \times 10^{-6} \text{ m}^2\right)^{-1} = 6.78 \text{ K/W}$$

The outlet temperature follows from Eq. (8.45b),

$$T_{m,o} = T_s - (T_s - T_{m,i}) \exp\left(-\frac{1}{\dot{m}_1 c_p R_{t,o}}\right) = 350\text{K} - (60\text{K}) \times \exp\left(-\frac{1}{10^{-4} \text{ kg/s} \times 4179 \text{ J/kg} \cdot \text{K} \times 6.78 \text{ K/W}}\right) = 307.8\text{K} \quad <$$

The heat rate per channel is then

$$q_1 = \dot{m}_1 c_p (T_{m,o} - T_{m,i}) = 10^{-4} \text{ kg/s} \times 4179 \text{ J/kg} \cdot \text{K} (17.8\text{K}) = 7.46 \text{ W}$$

and the chip power dissipation is

$$q = Nq_1 = 50 \times 7.46 \text{ W} = 373 \text{ W} \quad <$$

(b) The foregoing result indicates significant heat transfer from the channel side walls due to the large value of η_f . If the pitch is reduced by a factor of 2 ($S = 100 \mu\text{m}$), we obtain

$$S = 100 \mu\text{m}, W = 50 \mu\text{m}, \delta = 50 \mu\text{m}, N = 100: q_1 = 7.04 \text{ W}, q = 704 \text{ W} \quad <$$

Hence, although there is a reduction in η_f due to the reduction in δ ($\eta_f = 0.89$) and therefore a slight reduction in the value of q_1 , the effect is more than compensated by the increase in the number of channels. Additional benefit may be derived by further reducing the pitch to whatever minimum value of δ is imposed by manufacturing or structural limitations. There would also be an advantage to increasing the channel hydraulic diameter and or flowrate, such that turbulent flow is achieved with a correspondingly larger value of h .

COMMENTS: (1) Because electronic devices fail by contact with a polar fluid such as water, great care would have to be taken to hermetically seal the devices from the coolant channels. In lieu of water, a dielectric fluid could be used, thereby permitting contact between the fluid and the electronics. However, all such fluids, such as air, are less effective as coolants. (2) With $L/D_h = 125$ and $L/D_h)_{fd} \approx 0.05 \text{ Re}_D \text{ Pr} = 273$, fully developed flow is not achieved and the value of $h = h_{fd}$ underestimates the actual value of \bar{h} in the channel. The coefficient is also underestimated by using a Nusselt number that presumes heat transfer from all four (rather than three) surfaces of a channel.